

















So $J_1 = h_g(C_g - C_s)$, $J_2 = D_{O_2} \frac{C_o - C_i}{t_{ox}}$, & $J_3 = k_s C_i$, where k_s = chemical rate constant Continuity : $J = J_1 = J_2 = J_3$ gives 2 equations in 3 unknowns : C_s , C_o , C_i $h_g(C_g - C_s) = D_{O_2} \frac{C_o - C_i}{t_{ox}} = k_s C_i$ Add Henry's Law : $C_o = Hp_g = HkTC_s$, where H is a segregation coefficient, then solving gives $C_i = \frac{Hp_g}{1 + \frac{k_s}{h} + \frac{k_s t_{ox}}{D_{O_2}}}$ where $h = \frac{h_g}{HkT}$ and growth rate $R = \frac{J}{N_1} = \frac{k_s C_i}{N_1} = \frac{dt_{ox}}{dt} = \frac{Hk_s p_g}{N_1 \left[1 + \frac{k_s}{h} + \frac{k_s t_{ox}}{D_{O_2}} \right]}$ where N_1 = oxidant molecule density in grown oxide $= 2.2 \times 10^{22}$ /cc for O_2 and 4.4×10^{22} /cc for H_2O

$$\frac{dt_{ox}}{dt} = \frac{Hk_s p_g}{N_1 \left[1 + \frac{k_s}{h} + \frac{k_s t_{ox}}{D_{O_2}}\right]} \text{gives } N_1 \int_{t_i}^{t_{ox}} \left[1 + \frac{k_s}{h} + \frac{k_s t_{ox}}{D_{O_2}}\right] dt_{ox} = Hk_s p_g \int_{0}^{t} dt$$
with solution $\frac{N_1}{Hk_s p_g} \left[\left(1 + \frac{k_s}{h}\right) \left[t_{ox} - t_i\right] + \left(\frac{k_s}{2D_{O_2}}\right) \left[t_{ox}^2 - t_i^2\right] \right] = t$
 $\frac{\left[t_{ox} - t_i\right]}{B/A} + \frac{\left[t_{ox}^2 - t_i^2\right]}{B} = t \rightarrow \frac{t_{ox}^2}{B} + \frac{t_{ox}}{B/A} = t + \tau$
where t_i and $\tau = \frac{t_i^2 + At_i}{B}$ acount for any initial oxide thickness.
The quadratic solution is $t_{ox} = \frac{A}{2} \left[\sqrt{1 + \frac{t + \tau}{A^2/4B}} - 1 \right]$ with two limiting solutions :
 $t_{ox} \approx \frac{B}{A} (t + \tau)$ for small t_{ox} , and $t_{ox}^2 \approx B(t + \tau)$ for large t_{ox}
B/A and B are referred to as the linear and parabolic rate constants



• Under steady state conditions, F₁ = F₂ = F₃ so

$$C_{I} = \frac{C^{*}}{1 + \frac{k_{S}}{h} + \frac{k_{S}x_{O}}{D}} \cong \frac{C^{*}}{1 + \frac{k_{S}x_{O}}{D}}$$
(7)

$$C_{O} = \frac{C^{*}\left(1 + \frac{k_{S}x_{O}}{D}\right)}{1 + \frac{k_{S}}{h} + \frac{k_{S}x_{O}}{D}} \cong C^{*}$$
(8)

- Note that the simplifications are made by neglecting F₁ which is a very good approximation.
- Combining (6) and (7), we have

$$\frac{dx}{dt} = \frac{F}{N_1} = \frac{k_S C^*}{N_1 \left(1 + \frac{k_S}{h} + \frac{k_S x_O}{D}\right)}$$
(9)

• Integrating this equation, results in the linear parabolic model.

 $\frac{x_{\rm O}^2 - x_{\rm i}^2}{B} + \frac{x_{\rm O} - x_{\rm i}}{B/A} = t$ (10)

where
$$B = \frac{2DC}{N_1}$$
 (parabolic rate constant) (11)

and
$$\frac{B}{A} = \frac{C^*}{N_1\left(\frac{1}{k_s} + \frac{1}{h}\right)} \cong \frac{C^*k_s}{N_1}$$
 (linear rate constant) (12)

• (10) can also be written with oxide thickness as a function of time.

$$x_{0} = \frac{A}{2} \left\{ \sqrt{1 + \frac{t + \tau}{A^{2} / 4B}} - 1 \right\}$$
(13)

where $\tau = \frac{x_i^2 + Ax_i}{B}$ (14)

and
$$\frac{dx}{dt} = \frac{B}{A+2x_0} \rightarrow \frac{B}{A+2x_0} + Ce^{-x_o/L}$$
 for simulations (Massoud et al)

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Stagnat	e constants A & B in terms of C* than C _{o,} i.e. related to p _G depends on x
∴Redo basic theory:	$dx/dt = F_3/N_1 = (DC_0/N_1) / (x+D/k_s)$
	$(= k_{s}C_{i}/N_{1})$ =(D/N_{1})(1+k_{s}x/D)C*/(D/k_{s})(1+k_{s}x/D)(1+k_{s}x/D+k_{s}'h) = k_{s} (C*/N_{1}) / (1+k_{s}x/D+k_{s}'h) $\therefore (k_{s}/D) xdx + (1+k_{s}'h) dx = (k_{s}C*/N_{1}) dt$ (k_{s}/2D)x ² + (1+k_{s}'h)x = (k_{s}C*/N_{1})t + constant
	Boundary condition at t=0:
	constant = $(k_s x_i^2 / 2D) + (1 + k_s / h)x_i$
	= $k_s C^* \tau / N_1$ as definition of τ
	i.e. $\tau = (N_1/C^*) [x_i^2/2D + x_i(1/k_s + 1/h)]$
	$\therefore x^2 + 2D(1/k_s + 1/h)x - (2DC^*/N_1)(t + \tau) = 0$
	giving x= D (1/k _s + 1/h) x [{1+2C*(t+ τ) / N ₁ D (1/k _s + 1/h) ² } ^{1/2} -1]

Stagnation Layer #3





















B. Thin Oxide Growth Kinetics

- A major problem with the Deal Grove model was recognized when it was first proposed it does not correctly model thin O₂ growth kinetics.
- Experimentally O_2 oxides grow much faster for ≈ 20 nm than Deal Grove predicts
- MANY models have been suggested in the literature.

1. Reisman et. al. Model

$$\mathbf{x}_{\mathrm{O}} = \mathbf{a} \left(\mathbf{t} + \mathbf{t}_{\mathrm{i}} \right)^{\mathrm{b}} \quad \text{or} \quad \mathbf{x}_{\mathrm{O}} = \mathbf{a} \left(\mathbf{t} + \left(\frac{\mathbf{x}_{\mathrm{i}}}{\mathbf{a}} \right)^{\mathrm{b}} \right)^{\mathrm{b}}$$
(17)

• Power law "fits the data" for all oxide thicknesses.

- a and b are experimentally extracted parameters.
- Physically interface reaction controlled, volume expansion and viscous flow of SiO₂ control growth.

2. Han and Helms Model

$$\frac{\mathrm{dx}_{0}}{\mathrm{dt}} = \frac{\mathrm{B}_{1}}{2\mathrm{x}_{0} + \mathrm{A}_{1}} + \frac{\mathrm{B}_{2}}{2\mathrm{x}_{0} + \mathrm{A}_{2}} \tag{18}$$

- Second parallel reaction added "fits the data" " for all oxide thicknesses.
- Three parameters (one of the A values is 0).
- Second process may be outdiffusion of O_V and reaction at the gas/SiO₂ interface

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Thickness measurement by color

	$2n_{ox}$	T
Color	SiO ₂ thickness (nm)	Si ₃ N ₄ thickness (nm)
Silver	<27	<20
Brown	<53	<40
Yellow-brown	<73	<55
Red	<97	<73
Deep blue	<100	<77
Blue	<120	<93
Pale blue	<130	<100
Very pale blue	<150	<110
Silver	<160	<120
Light yellow	<170	<130
Yellow	<200	<150
Orange-red	<240	<180
Red	<250	<190
Dark red	<280	<210
Blue	<310	<230
Blue-green	<330	<250
Light green	<370	<280
Orange-yellow	<400	<300
Bed	<440	<330



























































Anodization: Growth Kinetics

 I_d = equivalent current to stop dissolution

 $\begin{array}{ll} \mbox{Formation:} & V_a \mbox{-} V_r = i \ (R_s \mbox{+} R_a) \mbox{+} V_{OX} \\ & = i \ (R_s \mbox{+} R_a \mbox{+} \alpha \ E_{OX} \ 0^{[t} \ i \ dt) \\ \mbox{Vr} \ = \ "rest \ potential" \ of \ cell \\ i.e. \ reverse \ emf \ of \ cell \ used \ by \ battery \end{array}$

 $\begin{array}{ll} \text{Try solution: i = I_0 exp - t / \tau} & \text{Note: i} \\ \text{So } _0^{[t]} \text{ i dt = - } \tau \text{ I}_0 [exp - t / \tau \ - 1] \\ \& \text{ V}_A - \text{ V}_R = (I_0 exp - t / \tau)(\text{R}_S + \text{R}_a) + \alpha \text{ E}_{OX}(1 - exp - t / \tau \] \tau \text{ I}_0 \\ \text{At t=0, } I_0 = (\text{V}_A - \text{V}_r)/(\text{R}_S + \text{R}_a) \\ \& \text{ at t=->} \infty, \text{ V}_A - \text{V}_r = \alpha \text{ E}_{OX} \tau \text{ I}_0 \\ \therefore \ \tau = (\text{V}_A - \text{V}_r) / \text{ I}_0 \alpha \text{ E}_{OX} = (\text{R}_S + \text{R}_a) / \alpha \text{ E}_{OX} \end{array}$

Growth Rate α i

Compare capacitor:

 $\begin{array}{ll} dv_c/dt \; \alpha \; i_c, & i_c = I_0 \; e^{-t/\tau}, \\ v_c(t) = V(1 - e^{-t/\tau}) \\ \therefore \; x = x_\infty(1 - \exp - t \; / \; \tau \;) \end{array}$

Final film thickness x_{∞} when no net growth

i.e. growth rate = dissolution rate, i=0 x_{∞} = (1 - I_d/I_0) (V_A-V_r) / E_{OX} \sim 0.3nm/volt for Si

i.e. control final thickness with voltage

Note: if I_d=0, no dissolution --> $x_{\infty} E_{OX}=V_A-V_r$ if I_d=I₀, no growth --> x_{∞} = 0

Anodization: Notes	
W (gms Si consumed/C) = W _e / qN	
- W _e = electrochemical equivalent weight	
= gm molec wt / valence charge in reaction	
-qN = 1.6x10 ⁻¹⁹ x 6.023x10 ²³ C/mole	
Current efficiency = experimental W / theoretical W	
\approx 95% for GaAs, \approx 1-3% for Si	
Can oxidize with constant current> dx/dt constant	
- for E_{OX} const, $V_{OX}\alpha$ x and increases linearly	
- monitor V_{OX} and stop at desired thickness	
Anodized SiO ₂	
- porous, etches 5x faster than thermal oxide	
- trapped H ₂ O can be reduced by heating	
- interface charge states 10x thermal oxide	
(no good for MOS)	

Anodization: Plasma

See later for plasmas High energy in plasma (electron temperature ≈ 10⁴ K) But low temperature in Si ∴ minimal dopant redistribution SiO₂ not as good as thermal



• Thermal oxidation has been a key element of silicon technology since its inception.

• Thermally, chemically, mechanically and electrically stable SiO₂ layers on silicon distinguish silicon from other possible semiconductors.

- The basic growth kinetics of SiO₂ on silicon are controlled by oxidant diffusion and Si/SiO₂ interface chemical reaction.
- This simple Deal-Grove model has been extended to include 2D effects, high dopant concentrations, mixed ambients and thin oxides.
- Oxidation can also have long range effects on dopant diffusion (OED or ORD) which are modeled through point defect interactions.
- Process simulators today include all these physical effects (and more) and are quite powerful in predicting oxidation geometry and properties.

Anodization is also possible.

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