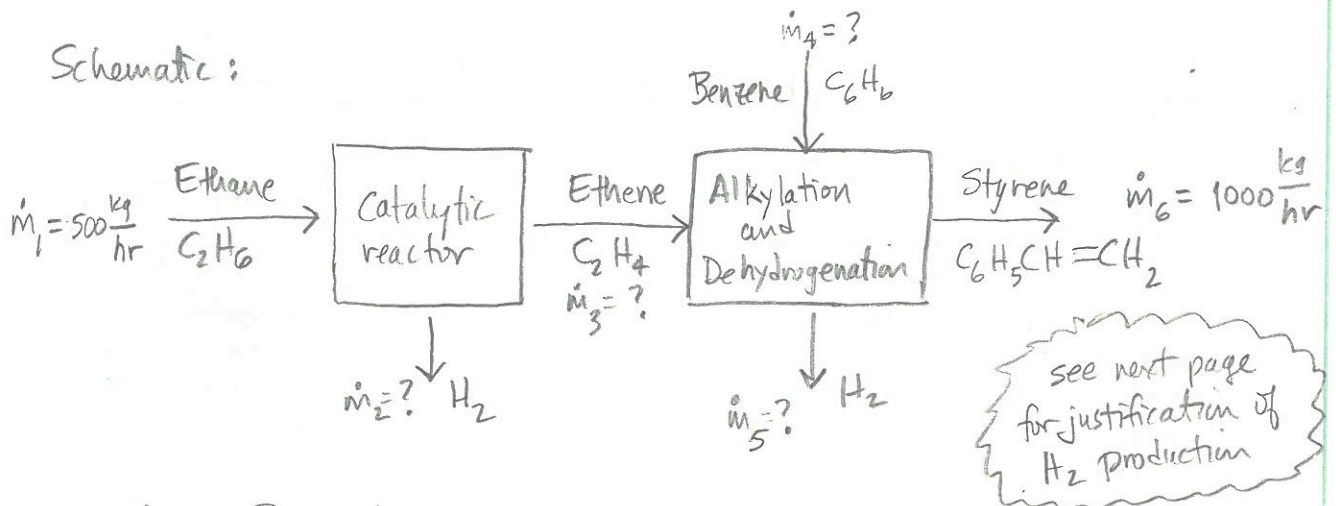


## Styrene mass balance problem

Step 1GIVEN: Available supply of ethane:  $\dot{m}_{C_2H_6} = 500 \text{ kg/hr}$ Desired production of styrene:  $\dot{m}_{\text{styrene}} = 1000 \text{ kg/hr}$ FIND: Required supply of Benzene:  $\dot{m}_{C_6H_6} = ?$ Rate of  $H_2$  production:  $\dot{m}_{H_2} = ?$ Step 2

Schematic:



Known Parameters:

$$\dot{m}_1 = 500 \frac{\text{kg}}{\text{hr}} = \text{mass flow rate of Ethane (input)}$$

$$\dot{m}_6 = 1000 \frac{\text{kg}}{\text{hr}} = \text{mass flow rate of Styrene (output)}$$

$$M_H = 1 \frac{\text{kg}}{\text{kmol}} = \text{molar mass of H}$$

$$M_C = 12 \frac{\text{kg}}{\text{kmol}} = \text{molar mass of C}$$

$$\Rightarrow M_{C_2H_6} = 2 \times 12 + 6 \times 1 = 30 \frac{\text{kg}}{\text{kmol}} = \text{molar mass of Ethane}$$

$$M_{C_2H_4} = 2 \times 12 + 4 \times 1 = 28 \frac{\text{kg}}{\text{kmol}} = \text{molar mass of Ethene}$$

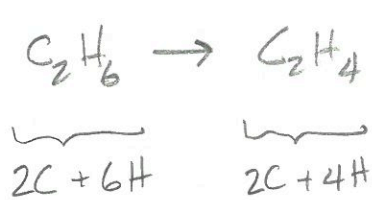
$$M_{C_6H_6} = 6 \times 12 + 6 \times 1 = 78 \frac{\text{kg}}{\text{kmol}} = \text{molar mass of Benzene}$$

$$M_{C_6H_5CH=CH_2} = 8 \times 12 + 8 \times 1 = 104 \frac{\text{kg}}{\text{kmol}} = \text{molar mass of Styrene}$$

SIDEBAR: How do you know that  $H_2$  is produced by the two reactions in the schematic?

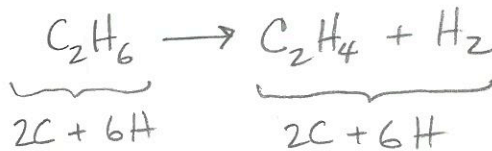
To answer that question, consider each reaction separately.

① Catalytic production of Ethene from Ethane

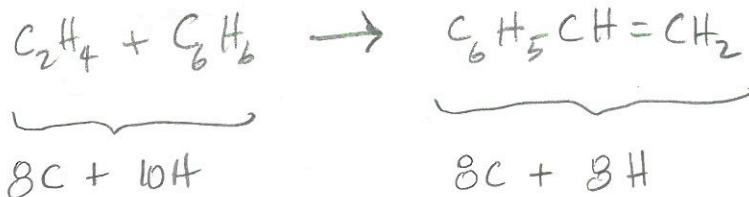


As written here, there is an imbalance in the number of Hydrogen atoms on the two sides of the reaction

To balance the reaction,  $H_2$  must be produced



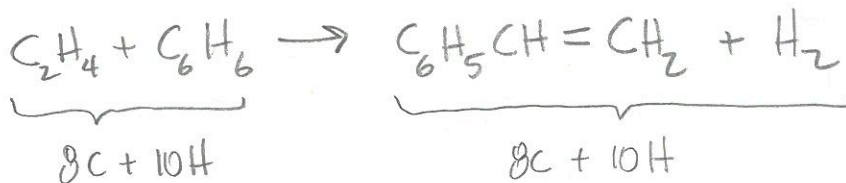
② Alkylation of Ethene and Benzene to form Styrene



NOT Stoichiometric

The left hand side (reactants) have 2 more H atoms than the right hand side

To balance the reaction,  $H_2$  must be produced



Unknowns:  $\dot{m}_2 = \text{H}_2$  production from the catalytic converter

$\dot{m}_5 = \text{H}_2$  production from the Alkylation and Dehydrogenation reaction

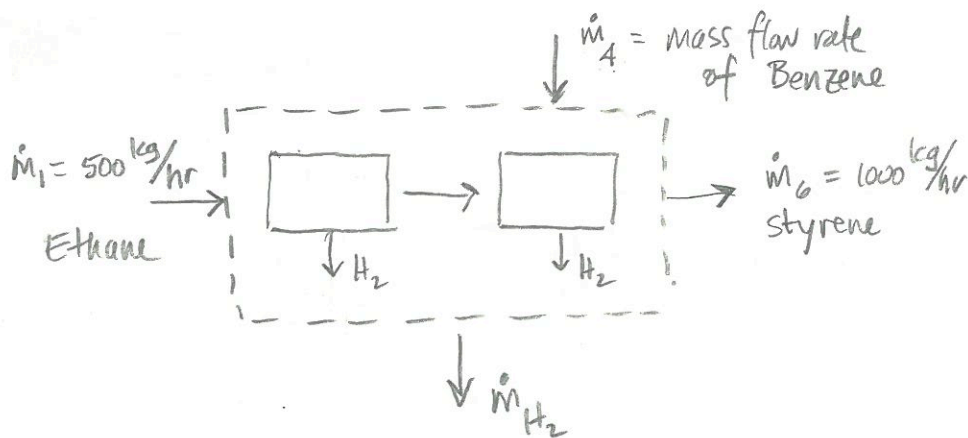
Note: Only  $\dot{m}_2 + \dot{m}_3 = \dot{m}_{\text{H}_2} = \text{total H}_2$  production is needed

more unknowns:  $\dot{m}_3 = \text{flow rate of Ethene}$

$\dot{m}_4 = \text{required input flow rate of Benzene}$

Key Observation: We only need to find the total rate of  $\text{H}_2$  production and the required input of Benzene. We are not interested in the intermediate product, Ethene.

Therefore, we can treat the two reactions as a single process. Redraw the system schematic.



This new schematic shows the two unknowns  $\dot{m}_4$  and  $\dot{m}_{\text{H}_2}$

Step 4

This is a steady flow process

There is no generation or consumption of the material, i.e. the total mass of H and total mass of C are conserved.

$$\Rightarrow \dot{m}_{\text{in}} = \dot{m}_{\text{out}} \text{ overall and for C and H}$$

Step 5:

Overall Mass Balance

$$\dot{m}_{in} = \dot{m}_{out}$$

$$\dot{m}_{\text{Ethane}} + \dot{m}_{\text{Benzene}} = \dot{m}_{\text{H}_2} + \dot{m}_{\text{Styrene}}$$

or, using symbols

$$\dot{m}_1 + \dot{m}_4 = \dot{m}_{\text{H}_2} + \dot{m}_6 \quad (1)$$

Carbon Mass Balance:

In any stream, the mass flow rate of Carbon is equal to the total mass flow rate of that stream times the fraction of carbon in the stream.

Therefore, at the Ethane input

$$\dot{m}_{\text{C, Ethane}} = \frac{24}{30} \dot{m}_1$$

$$24 \frac{\text{kg}}{\text{kmol}} = \text{contribution of C to molar mass of } \text{C}_2\text{H}_6$$

$$30 \frac{\text{kg}}{\text{kmol}} = \text{molar mass of } \text{C}_2\text{H}_6$$

$\therefore$  The mass flow rate of carbon in the Ethane input stream is  $\frac{24}{30} \dot{m}_1$

Repeat the preceding analysis while performing a mass balance on the Carbon

$$\begin{array}{ccccccc} \frac{24}{30} \dot{m}_1 & + & \frac{72}{78} \dot{m}_4 & = & \phi \dot{m}_{\text{H}_2} & + & \frac{96}{104} \dot{m}_6 & (2) \\ \uparrow & & \uparrow & & \uparrow & & \uparrow & \\ \text{Ethane} & & \text{Benzene} & & \text{Hydrogen} & & \text{Styrene} & \end{array}$$

Step 6

Equations (1) and (2) are two equations for the two unknowns  $\dot{m}_4$  and  $\dot{m}_{H_2}$

But, Equation (2) has only one unknown,  $\dot{m}_4$  (since the multiplier of  $\dot{m}_{H_2}$  is zero)

Solve Equation (2) for  $\dot{m}_4$

$$\frac{72}{78} \dot{m}_4 = \frac{96}{104} \dot{m}_6 - \frac{24}{30} \dot{m}_1$$

$$\dot{m}_4 = \frac{78}{72} \left( \frac{96}{104} \dot{m}_6 - \frac{24}{30} \dot{m}_1 \right)$$

$$= \frac{78}{72} \left[ \frac{96}{104} (1000 \frac{\text{kg}}{\text{hr}}) - \frac{24}{30} (500 \frac{\text{kg}}{\text{hr}}) \right]$$

$$\therefore \dot{m}_4 = 566.7 \frac{\text{kg}}{\text{hr}} \quad \text{mass flow rate of Benzene}$$

Substitute the value of  $\dot{m}_4$  into Equation (1) to solve for  $\dot{m}_{H_2}$

$$\dot{m}_{H_2} = \dot{m}_1 + \dot{m}_4 - \dot{m}_6$$

$$= 1000 \frac{\text{kg}}{\text{hr}} - 566.7 \frac{\text{kg}}{\text{hr}} - 500 \frac{\text{kg}}{\text{hr}}$$

$$\therefore \dot{m}_{H_2} = 66.7 \frac{\text{kg}}{\text{hr}} \quad \text{mass flow rate of } H_2$$

Step 7CHECK: Use  $H_2$  mass balance to check the computations

$$\frac{6}{30} \dot{m}_1 + \frac{6}{78} \dot{m}_4 = \dot{m}_{H_2} + \frac{8}{104} \dot{m}_6$$

↑
↑
←

Ethane                  Benzene                                  Styrene

$$\dot{m}_{in} = \dot{m}_{out} \Rightarrow \dot{m}_m - \dot{m}_{out} = 0$$

$$\frac{6}{30} \left( 500 \frac{\text{kg}}{\text{hr}} \right) + \frac{6}{78} \left( 566.7 \frac{\text{kg}}{\text{hr}} \right) - 66.7 \frac{\text{kg}}{\text{hr}} - \frac{8}{104} \left( 1000 \frac{\text{kg}}{\text{hr}} \right) \stackrel{?}{=} 0$$

$$100 \frac{\text{kg}}{\text{hr}} + 43.59 \frac{\text{kg}}{\text{hr}} - 66.7 \frac{\text{kg}}{\text{hr}} - 76.92 \frac{\text{kg}}{\text{hr}} \stackrel{?}{=} 0$$

$$-0.03 \frac{\text{kg}}{\text{hr}} \stackrel{?}{=} 0$$

OK with roundoff errors  
in the calculations